

# Enhancing electrochemical N<sub>2</sub> reduction at mild conditions with Fe<sub>x</sub>O<sub>y</sub> co-deposited on amorphous MoS<sub>2</sub>

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## ABSTRACT

Electrochemical reduction of N<sub>2</sub> can lead to the clean and sustainable production of NH<sub>3</sub> under environmental conditions. However, limited progress has been made as most catalysts lack efficient activity for N<sub>2</sub> fixation. Here, we report Fe<sub>x</sub>O<sub>y</sub> co-deposited on amorphous MoS<sub>2</sub> supported on a gas diffusion layer electrode (GDL) as an effective catalyst for N<sub>2</sub> reduction. The catalysts were prepared by electrodeposition, a simple and low-cost method. Physical characterizations revealed the amorphous nature of MoS<sub>2</sub> and while Fe<sub>x</sub>O<sub>y</sub> was evenly distributed over MoS<sub>2</sub>. In 0.1 M Na<sub>2</sub>SO<sub>4</sub>, GDL/MoS<sub>2</sub>-Fe-1 exhibited an NH<sub>3</sub> yield of 7.38 μmol h<sup>-1</sup> cm<sup>-2</sup>, a value almost 2 times greater than that obtained for MoS<sub>2</sub>/GDL and a faradaic efficiency of 54.9 % at -0.2 V vs. reversible hydrogen electrode (RHE) at 25 °C. Also, the catalyst displayed high stability and durability, retaining almost 93 % of its original values after recycling tests. The amorphous MoS<sub>2</sub>-Fe<sub>x</sub>O<sub>y</sub> provides new insight into designing efficient and robust catalysts for nitrogen reduction.

## 1. Introduction

The production of NH<sub>3</sub> is crucial for human development and the global economy, as ammonia is the second most synthesized chemical in the world [1,2]. In addition, ammonia is a promising carbon-free energy carrier with a high hydrogen content (17.6 % by mass), high energy density (4.25 kWh L<sup>-1</sup>), and easy handling and transport [3,4].

Currently, the production of NH<sub>3</sub> on a world scale depends on the Haber-Bosch (H-B) process, developed in the early 20th century. However, to increase the reaction rate, the industrial synthesis of ammonia is carried out at high temperatures (400–600 °C) and pressures (20–40 MPa) [1,4]. Furthermore, the H-B process requires a pure H<sub>2</sub> precursor mainly derived from natural gas reform [5,6]. As a result, the annual synthesis of NH<sub>3</sub> consumes about 1–2 % of global electrical energy and is responsible for approximately 3 % of global CO<sub>2</sub> [7].

Thus, researchers have been developing technologies capable of using H<sub>2</sub>O to replace H<sub>2</sub> as a source of protons to produce NH<sub>3</sub> at room temperature and atmospheric pressure [8]. An electrochemical approach to the nitrogen reduction reaction (NRR) to ammonia is a promising ecological and sustainable process to replace the Haber-Bosch process [8,9]. However, the high N≡N bond energy (940.95 kJ mol<sup>-1</sup>) in competition with the strong hydrogen evolution reaction (HER) poses substantial obstacles to reaction kinetics and

Faradaic efficiency (FE) in the NRR process [10,11]. In this regard, a great effort has been made to design low-priced, yet active and stable electrocatalysts to facilitate the NRR and restrain the undesired HER.

Mo and Fe are important elements in the enzyme nitrogenase due to the active site called iron-molybdenum cofactor (FeMoco), responsible for catalyzing N<sub>2</sub> fixation under environmental conditions in various biological systems [12]. Inspired by nature, several Fe-based [13–15] and Mo-based [16–18] catalysts have been employed for the electrochemical NRR. Among them, MoS<sub>2</sub> is a promising NRR candidate due to its tunable electronic structure and abundant edge active sites [16]. Nonetheless, the NRR performance of most existing MoS<sub>2</sub>-based catalysts is still far less satisfactory due to their limited available edge sites and the competition from the HER, which mostly prevented effective electron transfer for the NRR [17].

The addition of co-catalysts has been considered an effective strategy for improving the electrocatalytic performance of MoS<sub>2</sub> materials. A theoretical study has shown that the Fe-deposited MoS<sub>2</sub> sheets exhibit higher selectivity for N<sub>2</sub> fixation due to the strong electron interaction between Fe and MoS<sub>2</sub> [19]. For example, Zhao et al. [12] reported Fe nanodot-decorated MoS<sub>2</sub> nanosheets on carbon cloth (Fe-MoS<sub>2</sub>/CC) as a catalyst for NRR. The as-obtained material showed an average NH<sub>3</sub> yield of 12.5 μg h<sup>-1</sup> cm<sup>-2</sup> and a faradaic efficiency of 10.8 % at -0.1 V vs RHE, values 3.15 and 6.4 times higher, respectively, for the MoS<sub>2</sub>/CC

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electrode.

Besides, Fe oxide species (such as FeO and Fe<sub>2</sub>O<sub>3</sub>) can enhance the NRR due to their excellent redox property caused by the easy gain and loss of electrons in the d shell of the metal cations [20,21]. In this sense, Ma and co-workers [21] showed experimentally and theoretically, that Fe<sub>2</sub>O<sub>3</sub> nanoparticles anchored on MoS<sub>2</sub> nanoflowers (Fe<sub>2</sub>O<sub>3</sub>@MoS<sub>2</sub>) can enhance the NRR performance of MoS<sub>2</sub>. According to DFT calculations, Fe<sub>2</sub>O<sub>3</sub>@MoS<sub>2</sub> is better able to activate N<sub>2</sub> molecules compared to MoS<sub>2</sub>, as reflected by its lower energy barrier and greater charge transfer from active sites to N<sub>2</sub> molecules.

Amorphous materials have a nonperiodic structure of the internal arrangement of atoms or molecules. Their abundant defects in both surface and bulk as well as unique electronic properties make them promising candidates for electrochemical NRR [19]. Hence, increasing the concentration of edge layer sites of MoS<sub>2</sub> is another approach to enhance its NRR activity since the MoS<sub>2</sub> basal plane is inert for N<sub>2</sub> electroreduction [19].

An amorphous structure of MoS<sub>2</sub> presents a greater concentration of the edges layer sites compared to crystalline MoS<sub>2</sub> and, therefore, can provide abundant unsaturated coordination sites and surface-exposed defects, which provide active sites to capture and activate the N<sub>2</sub> molecule [22]. Moreover, amorphous materials are generally prepared at milder temperatures and with faster solidification processes than crystalline materials. The simple preparation methods, together with the low cost of the precursor materials, make this class of catalysts very attractive for the development of electrochemical and photoelectrochemical NH<sub>3</sub> production devices [23].

So far, the use of amorphous catalysts for the electrochemical reduction of N<sub>2</sub> is scarce in the literature. This work offers a promising opportunity to investigate amorphous MoS<sub>2</sub> for N<sub>2</sub> fixation. Thus, we report Fe<sub>x</sub>O<sub>y</sub> co-deposited on amorphous MoS<sub>2</sub> supported on a gas diffusion layer electrode (GDL) as an effective catalyst for the NRR. At 0.1 M Na<sub>2</sub>SO<sub>4</sub>, GDL/MoS<sub>2</sub>-Fe-1 exhibited a remarkable NH<sub>3</sub> yield of 7.38 μmol h<sup>-1</sup> cm<sup>-2</sup>, a value almost 2 times greater than that obtained for MoS<sub>2</sub>/GDL and a faradaic efficiency of 54.9 % at -0.2 V vs. RHE.

## 2. Experimental section

### 2.1. Chemicals

Ammonium tetrathiomolybdate ([NH<sub>4</sub>]<sub>2</sub>MoS<sub>4</sub> - 99.97 %), Sodium perchlorate (NaClO<sub>4</sub> - ≥ 98 %), Anhydrous sodium sulfate (NaSO<sub>4</sub> - ≥99.0 %), Iron (II) Chloride (FeCl<sub>2</sub> 4H<sub>2</sub>O - 98 %), para-(dimethylamino) benzaldehyde (p-C<sub>6</sub>H<sub>11</sub>NO), ascorbic acid (C<sub>6</sub>H<sub>8</sub>O<sub>6</sub> - ≥ 99 %), ammonium chloride (NH<sub>4</sub>Cl - 99.5 %), hydrazine hydrate (N<sub>2</sub>H<sub>4</sub> 80 % solution in H<sub>2</sub>O), concentrated hydrochloric acid (HCl - 37 wt%) sulfuric acid (H<sub>2</sub>SO<sub>4</sub> - 98 %), nitric acid (HNO<sub>3</sub> - 65 %) and phosphoric acid (H<sub>3</sub>PO<sub>4</sub> - 85 % in H<sub>2</sub>O) were purchased from Merck KGaA, Brazil. Ethanol (C<sub>2</sub>H<sub>5</sub>OH, 99.7 %) was purchased from Teda Inc. All reagents were of analytical grade and used without further purification. A gas diffusion layer (GDL - TGP-H-090 Wet proofed) was obtained from Toray Industries. Milli-Q ultrapure water (18.2 MΩ cm) was used in the preparation of all the solutions.

### 2.2. Pre-treatment of GDL

Before the deposition of the catalysts, the GDL substrate needed to be treated in acid to increase the hydrophilicity of the material, which is hydrophobic due to the presence of PTFE on its surface. For the acid treatment method, concentrated H<sub>2</sub>SO<sub>4</sub>/HNO<sub>3</sub> (V/V:3/1) solution were prepared. The GDL (0.5 × 0.5 cm) was dropped into the acid solution and subjected to an ultrasonic bath for 10 min at room temperature. Then, the substrate was rinsed copious times with ultrapure water and dried in the oven at 60 °C for 1 h.

### 2.3. Synthesis of amorphous MoS<sub>2</sub> (GDL/MoS<sub>2</sub>)

The molybdenum sulfide film was prepared by electrodeposition technique according to the literature [24,25]. Chronoamperometries (CA) were performed in the potential of -1.1 V for 60 min using 4 mmol L<sup>-1</sup> (NH<sub>4</sub>)<sub>2</sub>MoS<sub>4</sub> and 0.1 mol L<sup>-1</sup> NaClO<sub>4</sub> as the precursor solution previously deaerated with N<sub>2</sub> for 15 min. The GDL substrates (0.25 cm<sup>2</sup>) were used as the working electrode, while a Pt plate (1 cm<sup>2</sup>) and Ag/AgCl/Cl<sup>-</sup> (saturated with KCl) were the counter and reference electrodes, respectively.

### 2.4. Synthesis of amorphous MoS<sub>2</sub>-Fe (GDL/MoS<sub>2</sub>-Fe)

Fe was deposited over GDL/MoS<sub>2</sub> catalyst by electrodeposition. For this, a solution containing 50 mmol L<sup>-1</sup> FeCl<sub>2</sub> 4H<sub>2</sub>O and 10 mmol L<sup>-1</sup> ascorbic acid at pH 3.5 (with the addition of 1.0 mol L<sup>-1</sup> HCl) was used, previously deaerated with N<sub>2</sub> for 15 min. Electrodeposition was carried out at a constant potential of -1.0 V vs. Ag/AgCl/Cl<sup>-</sup> (saturated with KCl) and the time deposition was varied thus: 60, 150 and 300 s. The Fe deposition times were chosen to control the atomic proportion of Fe/(Mo+S) between the catalysts so that the effects of small (60 s) and high (300 s) amounts of Fe deposited on the catalyst were evaluated.

The same system with three electrodes, described in the item above, was used in these depositions. The catalysts were named GDL/MoS<sub>2</sub>-Fe-1, GDL/MoS<sub>2</sub>-Fe-2 and GDL/MoS<sub>2</sub>-Fe-3 according to the Fe deposition time, 60, 150 and 300 s, respectively. This nomenclature was used during the entire text.

### 2.5. Physical characterization

The crystalline structure was determined by X-ray diffraction (XRD) analysis performed using a BRUKER diffractometer model D8 ADVANCE, operating with Cu Kα radiation ( $k = 0.15406$  nm). The diffraction patterns were registered every 2θ angles from 20 to 90°, with a scan rate of 2° min<sup>-1</sup>. The crystallographic compositions of the catalysts through the X'Pert HighScore Plus program were compared with reference standards of the Joint Committee of Powder Diffraction Data Standards (JCPDS) database.

The morphology and film thickness were evaluated by dual-beam scanning electron microscopy (SEM) equipped with focused ion beam (FIB) observation equipment (FEI Vectra-IET). The composition of the films was studied by energy dispersive X-ray (EDX, FEI-XL30-FEG with Oxford Instruments-Link ISIS 300 detector). Laser Raman spectra were obtained using a Micro Raman Horiba iHR 550 spectrophotometer and a 532 nm laser.

The chemical surface analysis of the catalysts was realized by X-ray photoelectron spectroscopy (XPS) using a K-alpha XPS (Thermo Scientific) spectrometer with monochromatic Al Kα ( $h\nu = 1486$  eV) radiation as the excitation source. The binding energies (BE) were evaluated using the C 1 s spectrum (BE = 284.6 eV) as the reference. The spectra were fitted using CasaXPS (software version 2.3.15).

### 2.6. N<sub>2</sub> reduction reaction

The N<sub>2</sub> reduction reaction experiments were performed in an H-type electrocatalytic cell under ambient conditions. It consists of two cells separated by a Nafion™ membrane. The Nafion™ membrane was used as received, with no additional acid treatment. A counter electrode was placed in the anodic compartment, where the oxidation process generates protons. The reference electrode and working electrodes were placed in the cathodic compartment where the NRR takes place.

A potentiostat/galvanostat (Autolab Model PGSTAT 302 N) with a typical three electrode system was used to carry out all the electrochemical measurements. Herein, GDL/MoS<sub>2</sub>, GDL/Fe and GDL/MoS<sub>2</sub>-Fe were implemented as the working electrode, whereas a Pt plate (1 cm<sup>2</sup>) and an Ag/AgCl/Cl<sup>-</sup> (saturated with KCl) were implemented,

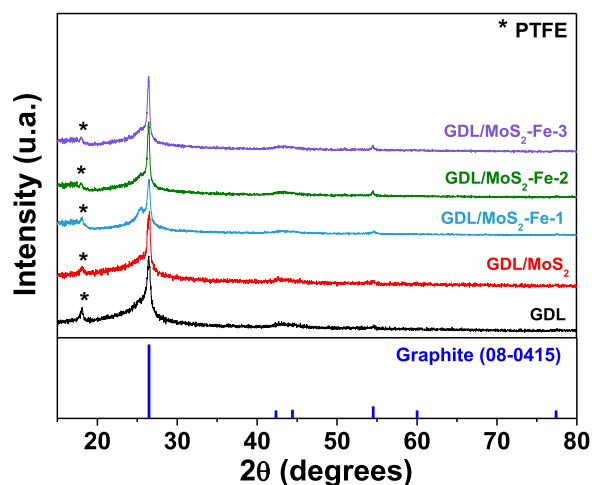


Fig. 1. X-ray diffraction patterns for GDL substrate, GDL/MoS<sub>2</sub> and GDL/MoS<sub>2</sub>-Fe catalysts.

respectively, as counter and reference electrodes. The potentials reported in the paper are expressed on the scale of the reversible hydrogen electrode (RHE) with the following equation:  $E$  (vs RHE) =  $E_{\text{appl}}$  (vs. Ag/AgCl/Cl<sup>-</sup> (sat. KCl)) +  $\text{pH} \times 0.059 \text{ V} + 0.197 \text{ V}$  [26]. Subsequently, the current density was recorded with respect to the geometric surface area of the working electrode.

The reaction was carried out in 60 mL (25 mL in the anodic compartment and 35 mL in the cathodic compartment) of 0.1 mol L<sup>-1</sup> Na<sub>2</sub>SO<sub>4</sub> in which high purity N<sub>2</sub> gas (99.999 %, 20 mL min<sup>-1</sup>) was bubbled for 45 min for complete saturation of the medium, as well as throughout the entire experiment (2 h). A 30 mL acid trap of 0.005 mol H<sub>3</sub>PO<sub>4</sub> [27] was connected to the cathodic compartment for ammonia storage. The reactions were reproduced in triplicate.

## 2.7. NH<sub>3</sub> detection

The yield amount of NH<sub>3</sub> ( $C[\text{NH}_3]_{\text{N}_2}$ ) in the solution was measured by a colorimetric indophenol blue method [28] using the Merck Spectroquant® commercial kit. Briefly, 5.0 mL aliquots were mixed with 0.6 mL of the NH<sub>4</sub>-1 reagent and a micro spoon of the NH<sub>4</sub>-2 reagent (as supplied in the kit), followed by stirring for 5 min and resting for 10 min for the complete reaction of the reagents. Then, 4 drops of the NH<sub>4</sub>-3 reagent were added to the aliquots followed by stirring for 5 min and standing for 20 min.

The prepared samples were then analyzed on a UV-vis Spectrometer (Varian, Cary 5 G UV-vis-NIR) at a wavelength of 690 nm. A calibration curve for NH<sub>3</sub> was constructed, using the procedure described above in triplicate, on standard NH<sub>4</sub>Cl solutions prepared in 0.1 mol L<sup>-1</sup> Na<sub>2</sub>SO<sub>4</sub> media with NH<sub>4</sub><sup>+</sup> concentrations ranging from 0.00 to 3.00 μg mL<sup>-1</sup>. A curve fit ( $y = 0.2998x + 0.0096$ ,  $R^2 = 0.99926$ ) of the three independent calibrations shows a good linear relationship between the absorbance value and the NH<sub>3</sub> concentration (Fig. S1).

To eliminate the possible exterior sources of contaminations [29] the corresponding Ar-saturated ( $C[\text{NH}_3]_{\text{Ar}}$ ) condition and the open-circuit N<sub>2</sub>-saturated condition ( $C[\text{NH}_3]_{\text{Open}}$ ) for the NRR experiment were used as the baseline for NH<sub>3</sub> production. Thus, the corrected  $C[\text{NH}_3]$  produced during the N<sub>2</sub> reduction was calculated using the following equation (Eq. (1)):

$$C[\text{NH}_3] = C[\text{NH}_3]_{\text{N}_2} - C[\text{NH}_3]_{\text{Ar}} - C[\text{NH}_3]_{\text{Open}} \quad (1)$$

The NH<sub>3</sub> yield rate was determined by (Eq. (2)):

$$\text{NH}_3 \text{ yield rate (mol h}^{-1} \text{ cm}^{-2}) = (C[\text{NH}_3] \times V)/(t \times A) \quad (2)$$

Where  $C[\text{NH}_3]$  is the corrected concentration of NH<sub>3</sub> production (mol

L<sup>-1</sup>);  $V$  is the volume of the electrolyte (L);  $A$  is the geometric surface area of the working electrode (cm<sup>2</sup>), and  $t$  is the electrolysis reaction time (h).

The faradaic efficiency (FE) can be calculated using the following equation (Eq. (3)):

$$FE = (3F \times C[\text{NH}_3] \times V)/Q \quad (3)$$

Where  $F$  refers to the Faraday constant (96,485.3 C mol<sup>-1</sup>),  $Q$  is the quantity of electric charge via the applied potential during the entire experiment (C).

## 2.8. N<sub>2</sub>H<sub>4</sub> detection

The Watt and Chrisp method was adopted to quantify the N<sub>2</sub>H<sub>4</sub> in the electrolyte after the reaction [30]. The coloring agent was prepared by mixing 6.0 g of p-C<sub>6</sub>H<sub>11</sub>NO with 30 mL of concentrated HCl and 300 mL of C<sub>2</sub>H<sub>5</sub>OH. Then, 5 mL of the electrolyte was taken from the acid trap and mixed with 5 mL of the coloring agent followed by stirring for 10 min and standing for 20 min. The absorbance of the solution was constructed using standard hydrazine hydrate solutions ranging from 0.2 to 1.2 μg mL<sup>-1</sup>. As demonstrated in Fig.S2, a good linear relationship ( $y = 0.7184x + 0.2456$ ,  $R^2 = 0.99939$ ) between the absorbance value and the N<sub>2</sub>H<sub>4</sub> concentration were obtained in three independent calibrations.

## 2.9. FTIR measurements

*In situ* FTIR measurements were carried out by using a Nicolet 6700 FTIR spectrometer (Thermo Fisher) equipped with MCT (Mercury-Cadmium-Telluride) detector cooled with liquid nitrogen. Spectra were computed from an average of 64 interferograms. The spectral resolution was set to 4 cm<sup>-1</sup>. The electrochemical infrared cell was fitted with a CaF<sub>2</sub> prismatic window. The catalyst was electrodeposited on a glassy carbon electrode (7 mm in diameter) previously polished to a mirror finish (alumina, 0.05 μm) to obtain good reflectivity. The reaction was carried out in 0.1 mol L<sup>-1</sup> Na<sub>2</sub>SO<sub>4</sub> in which high purity N<sub>2</sub> gas was bubbled for 45 min for complete saturation of the medium. The spectra were collected during chronoamperometry at -0.2 V vs RHE for 1000s.

## 3. Results and discussion

### 3.1. Physical characterization

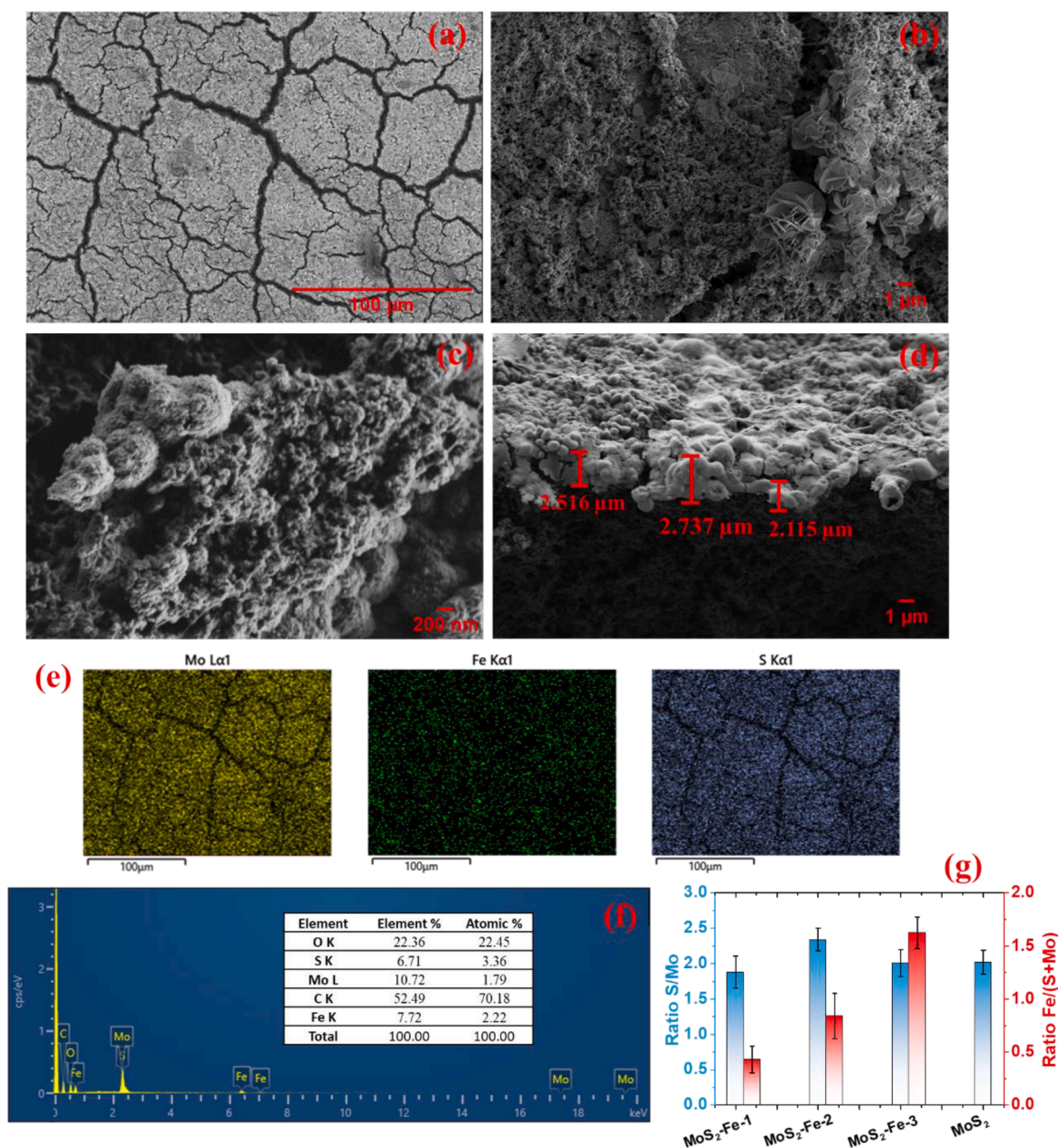
XRD analyzes were performed to identify the crystallographic structure of the GDL substrate and as-synthesized GDL/MoS<sub>2</sub> and GDL/MoS<sub>2</sub>-Fe catalysts. According to Fig. 1, the diffraction peaks at 26.4, 42.3, 44.5 and 54.6° corresponds to (002), (100), (101) and (004) planes of the GDL substrate (PDF No. 00-041-1487) [31]. The other peak located at 18.1° relates to PTFE (PDF No. 00-045-1594) [32].

On the other hand, no peaks for the molybdenum sulfide were detected. The absence of these characteristic diffraction peaks suggests the existence of MoS<sub>2</sub> in the amorphous phase, which is consistent with previous reports for MoS<sub>2</sub> prepared by electrodeposition [24,25]. In addition, the XRD patterns showed that for all the GDL/MoS<sub>2</sub>-Fe catalysts, no crystalline Fe or oxidized species peaks could be observed, indicating the amorphous nature of the Fe electrodeposited.

The morphology and chemical components of the catalysts are characterized by SEM/EDX, as illustrated in Fig. 2. SEM images for the GDL/MoS<sub>2</sub> (Fig. S3a-S3c) catalyst were taken at different magnifications and showed a globular form, typically for amorphous MoS<sub>2</sub> films, consistent with the XRD data (Fig. 1) [25,33].

Fig. 2a-2c illustrates the SEM images at different magnifications for GDL/MoS<sub>2</sub>-Fe-1. The Fe deposit (Fig. 2b) consists of a sheet-like structure. In contrast, the electrodeposition of Fe did not induce morphological changes in the MoS<sub>2</sub> film (Fig. 2c), with the typical globular form still observed.

However, increasing the Fe deposition time, the films become rough,



**Fig. 2.** (a, c) SEM images at different magnifications for GDL/MoS<sub>2</sub>-Fe-1. (d) GDL/MoS<sub>2</sub>-Fe-1 film thickness. Image obtained by a SEM equipped FEG observation equipment. (e) EDX elemental mapping distribution and (f) EDX spectrum with 500x magnification. (g) Elemental atomic ratio obtained by EDX.

and the sheet-like structure is more abundant, as observed in SEM images for GDL/MoS<sub>2</sub>-Fe-2 (Fig. S4a–S4c) and GDL/MoS<sub>2</sub>-Fe-3 (Fig. S5a–S5c) catalysts, indicating the successful deposition of Fe onto the MoS<sub>2</sub> films. Fig. 2d shows the results of the thickness value for three different regions of GDL/MoS<sub>2</sub>-Fe-1 film. The mean thickness of GDL/MoS<sub>2</sub>-Fe-1 film is about  $2.44 \pm 0.315 \mu\text{m}$ .

The presence of S, Mo, and Fe elements in the GDL/MoS<sub>2</sub>-Fe-1 film is observed from the EDX mappings in Fig. 2e, 2f. The same is observed in EDX mappings for GDL/MoS<sub>2</sub> (Fig. S3d), GDL/MoS<sub>2</sub>-Fe-2 (Fig. S4d) and GDL/MoS<sub>2</sub>-Fe-3 (Fig. S5d), demonstrating that the elements are evenly dispersed in the substrate.

EDX spectroscopy was performed to evaluate the atomic ratio of S/Mo and Fe/(S+Mo) in the catalysts (Figs. 2g and S6). Fig. 2g shows that the atomic ratio of S/Mo ranged between 1.88 and 2.34 and it was assumed that MoS<sub>2</sub> species were deposited [24,25,34,35]. The Fe/(S+Mo) atomic ratios show that the amount of Fe deposited grows continuously as the time of deposition increases. In addition, for all

catalysts, the stoichiometry between S/Mo was not lost with Fe deposition.

To further confirm the amorphous nature of the as-prepared catalysts, Raman scattering spectra are recorded and shown in Fig. S7. Spectra of GDL (Fig. S7a) presented a band at  $734 \text{ cm}^{-1}$  attributed to C-F symmetric stretching mode in PTFE. Besides, another band originated from the overlapping of two bands located at  $1380$  and  $1572 \text{ cm}^{-1}$  are related to the stretching of the C–C bond and the in-plane hexagonal vibrations of C–C in a graphitic structure [36].

For GDL/MoS<sub>2</sub> and GDL/MoS<sub>2</sub>-Fe-1 catalysts (Fig. S7b), Raman spectra revealed a poor definition of the characteristic peaks expected for crystalline MoS<sub>2</sub> [34,35], which suggests that crystalline MoS<sub>2</sub> is not present in significant quantities in the as-deposited catalyst and an amorphous MoS<sub>2</sub> and MoS<sub>2</sub>-Fe films were deposited.

The Raman spectrum analysis agrees with the XRD and SEM data, revealing the amorphous nature of the materials. GDL/MoS<sub>2</sub> exhibited two broad bands at  $321$  and  $417 \text{ cm}^{-1}$ , ascribed to the in-plane Mo-S

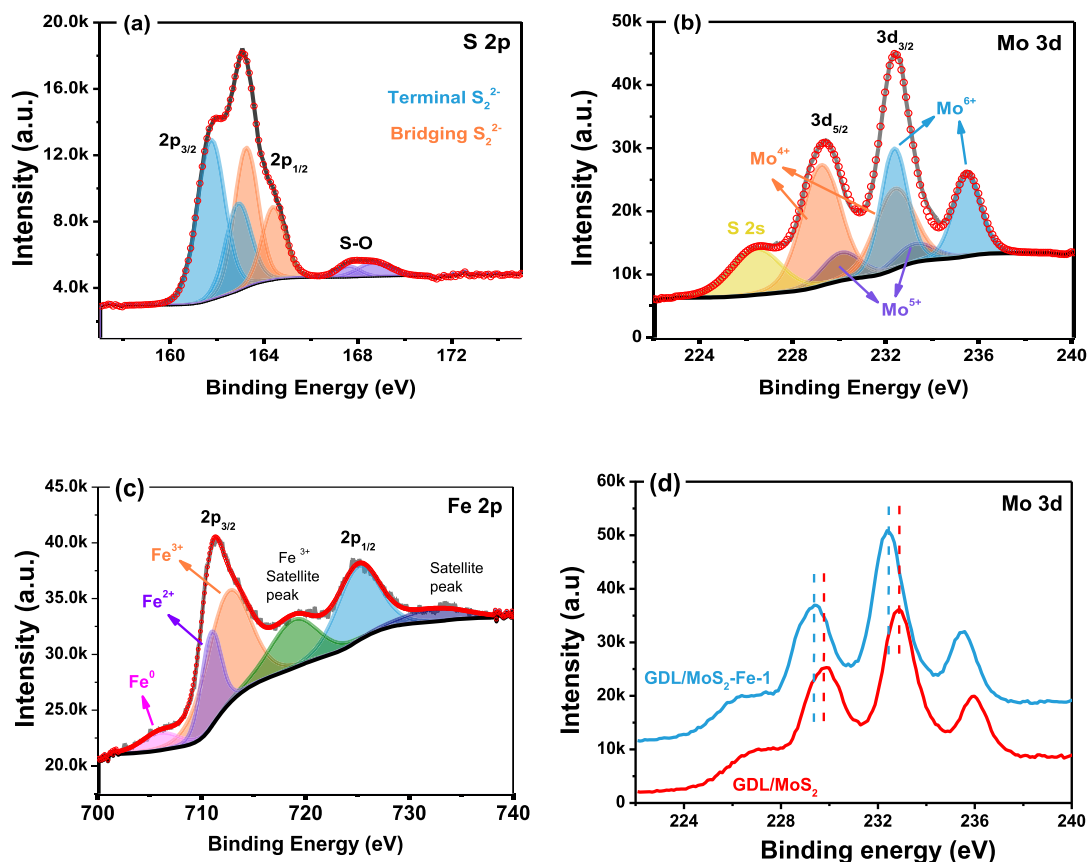


Fig. 3. High-resolution spectra of (a) Mo 3d, (b) S 2p and (c) Fe 2p of GDL/MoS<sub>2</sub>-Fe-1. (d) Displacement of the Mo 3d binding energies for GDL/MoS<sub>2</sub>-Fe-1 compared to GDL/MoS<sub>2</sub>.

mode ( $E_{2g}^1$ ) and the out-plane Mo-S mode ( $A_{1g}$ ), respectively [34–37]. A broad band located at 800–900  $\text{cm}^{-1}$  can be ascribed to MoO<sub>3</sub> was observed in all catalysts [38].

For GDL/MoS<sub>2</sub>-Fe-1 catalyst (Fig. S7b), another two bands appear at 211 and 274  $\text{cm}^{-1}$  that can be attached to  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub>, indicating that Fe is presented in the oxidized form [39,40]. Compared with those of GDL/MoS<sub>2</sub>, the vibrational bands of GDL/MoS<sub>2</sub>-Fe all showed displacement to lower values, indicating a chemical change in the Mo-S bond due to the electronic interaction between MoS<sub>2</sub> and Fe [12].

X-ray photoelectron spectroscopy (XPS) was used to verify the surface chemical composition and valence state of the S, Fe and Mo atoms on the MoS<sub>2</sub> and MoS<sub>2</sub>-Fe catalysts. Fig. 3a shows the survey XPS spectra for GDL/MoS<sub>2</sub> and GDL/MoS<sub>2</sub>-Fe catalysts. As expected, the survey scan spectrum (Fig. S8a) confirmed the presence of S, Fe, Mo, C, F and O elements in the catalysts.

According to Table S1, the S/Mo ratio for the MoS<sub>2</sub>/GDL film was 1.92/1, while for the MoS<sub>2</sub>-Fe-1 the S/Mo/Fe ratio was 2.11/1/0.42, which is very close to the stoichiometric MoS<sub>2</sub>, and agrees with the EDX spectroscopy (Fig. 2f).

The high-resolution XPS data in the S 2p region for GDL/MoS<sub>2</sub>-Fe-1 (Fig. 3a) and GDL/MoS<sub>2</sub> (Fig. S8b) are composed of terminal S<sub>2</sub><sup>2-</sup> and bridge S<sub>2</sub><sup>2-</sup> configurations each with two doublets [41]. The atomic percentages for the terminal S<sub>2</sub><sup>2-</sup> and bridge S<sub>2</sub><sup>2-</sup> configurations for GDL/MoS<sub>2</sub> (Table S2) were 48.4 % and 40.4 %, respectively. One more doublet related to sulfate (S-O) was identified in both catalysts.

However, after Fe deposition, there is a slight increase in the terminal S configuration to 53.7 %, indicating greater exposure of the lateral sites of the MoS<sub>2</sub>-Fe-1 catalyst [41–43]. As discussed before, the basal surface of MoS<sub>2</sub> is inert, although the edge of MoS<sub>2</sub> catalyst is active for N<sub>2</sub> electroreduction [19,20]. Thus, it is reasonable to assume that Fe

deposition can enhance GDL/MoS<sub>2</sub>-Fe catalytic activity and facilitate N<sub>2</sub> adsorption due to increasing the concentration of edge layer sites of MoS<sub>2</sub>.

The molybdenum region for GDL/MoS<sub>2</sub>-Fe-1 (Fig. 3b) and GDL/MoS<sub>2</sub> (Fig. S8c) was deconvoluted into three doublets (Mo 3d<sub>5/2</sub> and 3d<sub>3/2</sub>) equivalent to the Mo<sup>4+</sup>, Mo<sup>5+</sup> and Mo<sup>6+</sup> states [24,44]. The Mo 3d spectrum contains peaks due to Mo<sup>6+</sup> due to molybdenum oxysulfide, indicating the oxide formation during the synthesis or film oxidation during the storage. However, OH<sup>-</sup> is produced during cathodic deposition (Eq. (4)), which may facilitate the formation of this species [45]. Another peak is shown at 226.4 eV, which was attributed to S 2s [42].

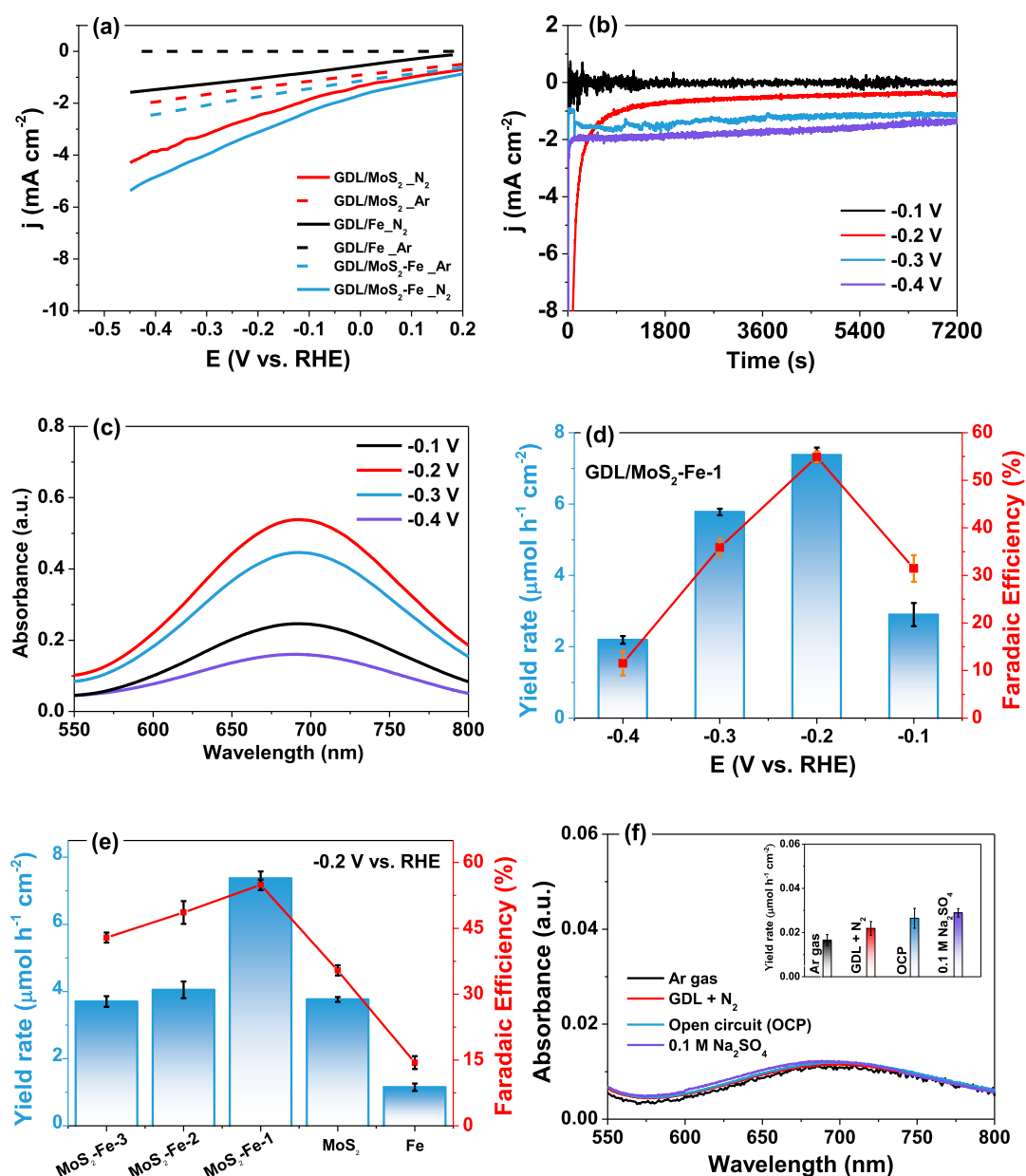


For GDL/MoS<sub>2</sub>-Fe-1, the binding energies of Mo 3d<sub>5/2</sub> and Mo 3d<sub>3/2</sub> show a negative shift after Fe deposition, as displayed in Fig. 3d. The electronic structure is directly related to the binding energy [12]. So, the binding energy displacement in the Mo XPS spectra suggests the electronic interaction between Fe and MoS<sub>2</sub>. Likewise, the binding energies of S 2p<sub>3/2</sub> and S 2p<sub>1/2</sub> for GDL/MoS<sub>2</sub>-Fe-1 also show a negative shift compared with those for GDL/MoS<sub>2</sub>, as shown in Fig. S8c.

### 3.2. NRR on GDL/MoS<sub>2</sub> and GDL/MoS<sub>2</sub>-Fe catalysts

To investigate the catalytic activity of GDL/MoS<sub>2</sub> and GDL/MoS<sub>2</sub>-Fe catalysts towards NRR, electrochemical experiments were conducted in N<sub>2</sub>-saturated 0.1 mol L<sup>-1</sup> Na<sub>2</sub>SO<sub>4</sub>. The NRR was performed in the neutral electrolyte Na<sub>2</sub>SO<sub>4</sub> to reduce the competitive H<sup>+</sup> adsorption in HER.

Fig. 4a shows the LSV curves at a scan rate of 10 mV s<sup>-1</sup> to determine the electrochemical window for the NRR over the materials. For all catalysts, there is an increase in the current density after the electrolyte



**Fig. 4.** (a) LSV curves of GDL/MoS<sub>2</sub>, GDL/Fe and GDL/MoS<sub>2</sub>-Fe-1 in 0.1 mol L<sup>-1</sup> Na<sub>2</sub>SO<sub>4</sub> electrolyte saturated with N<sub>2</sub> and Ar. (b) Time-dependent current density curves of GDL/MoS<sub>2</sub>-Fe-1 for NRR at different potentials (c) UV-vis absorption spectra stained with indophenol indicator at different potentials of GDL/MoS<sub>2</sub>-Fe-1 (d) NH<sub>3</sub> yield rates and FE at different potentials of GDL/MoS<sub>2</sub>-Fe-1. (e) NH<sub>3</sub> yield rates and FE for GDL/MoS<sub>2</sub>-Fe with different Fe deposition times, GDL/Fe and GDL/MoS<sub>2</sub> catalysts at -0.20 V vs. RHE. (f) UV-vis absorption spectra of the electrolytes stained with indophenol indicator at -0.20 V for 2 h under various conditions. The insert: NH<sub>3</sub> yield rates under various conditions.

has been purged with N<sub>2</sub>, indicating the occurrence of the NRR.

The time-dependent current density curves of the GDL/MoS<sub>2</sub>-Fe-1 catalyst at different potentials are shown in Fig. 4b, and 4c is relevant UV-vis absorption spectra of the electrolytes colored with the indophenol indicator at different potentials for 2 h. As shown in Fig. 4d, the NH<sub>3</sub> yield rates and FE initially increase as the electrolysis potential becomes more negative. However, as the potential moves below -0.2 V vs. RHE, the NH<sub>3</sub> yield rates and FE decrease rapidly, which might result from the competitive HER [12,46].

At -0.20 V vs. RHE, GDL/MoS<sub>2</sub>-Fe-1 presents the highest NH<sub>3</sub> average yield rate of 7.38 μmol h<sup>-1</sup> cm<sup>-2</sup>, a value almost 2 times greater than that obtained for GDL/MoS<sub>2</sub>, and a corresponding FE of 54.9%. A previous study has demonstrated that oxidized Fe species can improve water attraction and acts as a proton channel to promote N<sub>2</sub> reduction,

which can enhance the MoS<sub>2</sub> activity [20,47]. Besides, the Fe center can transfer electronic charges to MoS<sub>2</sub>, facilitating N<sub>2</sub> molecular adsorption and activation [17].

The possible N<sub>2</sub>H<sub>4</sub> production was detected by Watt and Chrisp method (Fig. S9a), but no detectable N<sub>2</sub>H<sub>4</sub> was observed for all catalysts at different potentials (Fig. S9b–9e). The result rules out the formation of hydrazine and signifies the formation of NH<sub>3</sub> only, indicating that the catalysts are selective for ammonia production.

To investigate the effect of Fe deposition on MoS<sub>2</sub> NRR, several GDL/MoS<sub>2</sub>-Fe, varying the Fe deposition time, were tested toward NRR. GDL/Fe was also synthesized to explore the effect between Fe and MoS<sub>2</sub>. The NRR performances of GDL/Fe after 2 h of potentiostatic electrolysis at different potentials are presented in Fig. S10a.

As shown in Fig. 4e, when the atomic ratio of Fe/(Mo+S) changed

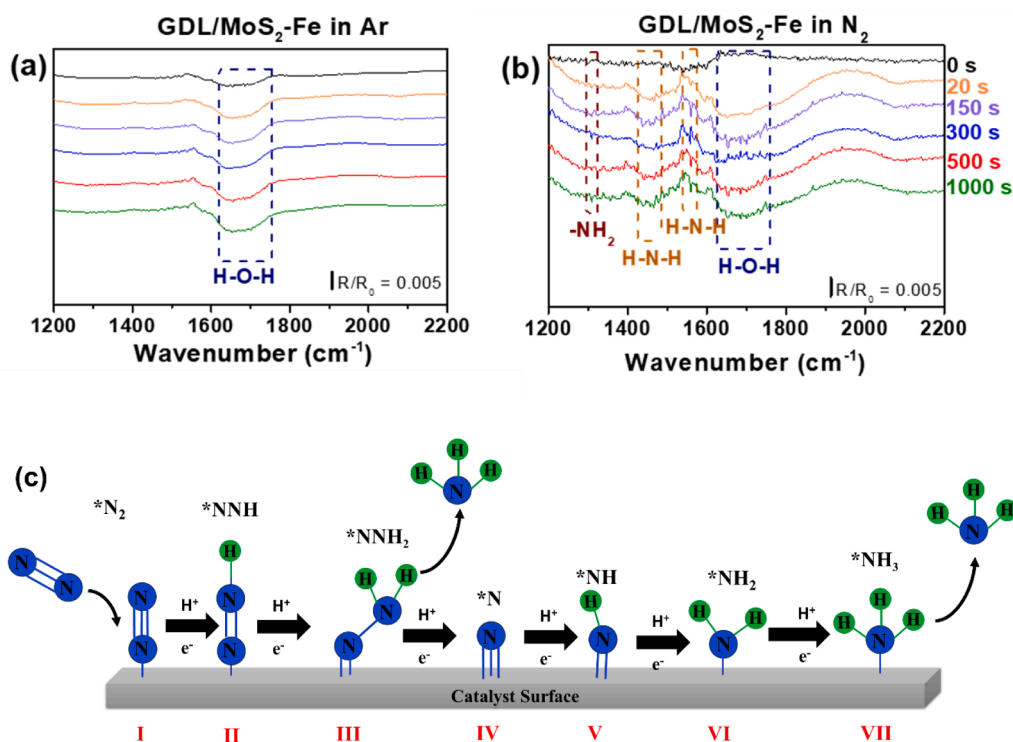


Fig. 5. Electrochemical *in situ* FTIR spectra of the NRR on the GDL/MoS<sub>2</sub>-Fe-1 catalysts at  $-0.2$  V vs RHE in (a) Ar and (b) N<sub>2</sub>. (c) Proposed NRR via an associative mechanism.

Table 1

A summary of the representative experimental studies on NRR using various electrocatalytic catalysts.

Catalyst	Electrolyte	Potential (V) vs. RHE	Detection method	NH <sub>3</sub> yield	Faradaic Efficiency (%)	Refs.
GDL/MoS <sub>2</sub> -Fe-1	0.1 M Na <sub>2</sub> SO <sub>4</sub>	$-0.2$	Indophenol blue	$2.07 \times 10^{-9}$ mol s <sup>-1</sup> cm <sup>-2</sup> (127.17 μg h <sup>-1</sup> cm <sup>-2</sup> )	54.9	This study
MoS <sub>2</sub> @Fe(OH) <sub>3</sub> 1D-MoS <sub>2-x</sub> O <sub>y</sub>	0.1 M Na <sub>2</sub> SO <sub>4</sub> 0.1 M HCl	$-0.45$	Indophenol blue	$4.23 \times 10^{-10}$ mol s <sup>-1</sup> cm <sup>-2</sup>	2.76	[20]
		$-0.35$	Indophenol blue	$5.56 \times 10^{-8}$ mol s <sup>-1</sup> cm <sup>-2</sup>	9.86	[55]
PAL-MoS <sub>2</sub>	0.1 M HCl	$-0.1$	Indophenol blue	$1.98$ μg h <sup>-1</sup> cm <sup>-2</sup>	44.36	[56]
1T-MoS <sub>2</sub> -Ni	0.25 M LiClO <sub>4</sub>	$-0.3$	Indophenol blue	$63$ μg h <sup>-1</sup> cm <sup>-2</sup>	27.66	[45]
Fe-MoS <sub>2</sub> /CC	0.1 M KOH	$-0.1$	Indophenol blue	$12.5$ μg h <sup>-1</sup> cm <sup>-2</sup>	10.8	[12]
Ru/2H-MoS <sub>2</sub>	0.01 M HCl	$-0.15$	Indophenol blue	$0.91 \times 10^{-10}$ mol s <sup>-1</sup> cm <sup>-2</sup> (5.6 μg h <sup>-1</sup> cm <sup>-2</sup> )	12.2	[57]
Fe-MoS <sub>2</sub>	0.1 M KCl	$-0.2$	ion chromatography	$97.5 \pm 6$ μg h <sup>-1</sup> cm <sup>-2</sup>	$31.6 \pm 2$	[58]
Mo SAs-Mo <sub>2</sub> C/ NCNTs	5 mM H <sub>2</sub> SO <sub>4</sub> + 0.1 M K <sub>2</sub> SO <sub>4</sub>	$-0.25$	ion chromatography and Indophenol blue	$16.1$ μg h <sup>-1</sup> cm <sup>-2</sup>	7.1	[59]

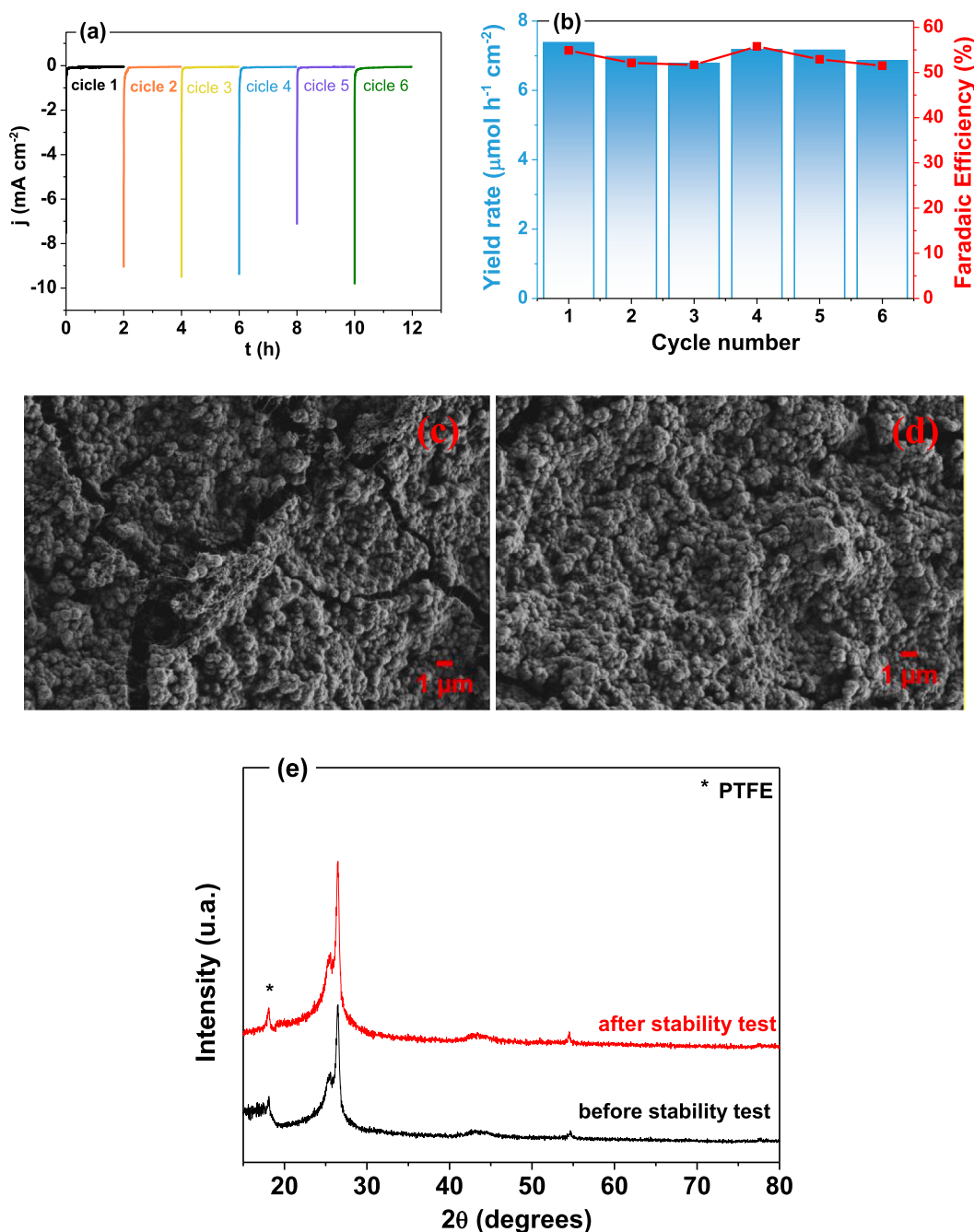
from 0.43 (GDL/MoS<sub>2</sub>-Fe-1) to 0.84 (GDL/MoS<sub>2</sub>-Fe-2), the NH<sub>3</sub> yield rates and FE decreased sharply. At a higher Fe/(Mo+S) atomic ratio (1.64) for GDL/MoS<sub>2</sub>-Fe-3, considering the standard deviation, the NH<sub>3</sub> yield rates and FE do not modify significantly. The NRR performances and the UV-vis absorption spectra of GDL/MoS<sub>2</sub>-Fe-2 and GDL/MoS<sub>2</sub>-Fe-3 after 2 h of potentiostatic electrolysis at different potentials are presented in Fig. S10c, S10d and Fig. S10e, S10f, respectively.

Additionally, GDL/Fe yields only a small amount of NH<sub>3</sub> and low FE compared to GDL/MoS<sub>2</sub> (Fig. S10g, S10h), which excludes the possibility that Fe/Fe<sub>x</sub>O<sub>y</sub> contributes as the leading active site for NRR in the GDL/MoS<sub>2</sub>-Fe catalyst. The results show that the improved NRR activity in the GDL/MoS<sub>2</sub>-Fe-1 catalyst originates from the synergistic effect between Fe and MoS<sub>2</sub>. However, higher concentrations of Fe/Fe<sub>x</sub>O<sub>y</sub> may cover MoS<sub>2</sub> film and therefore block its active sites, which explains the decrease in NRR performance at higher Fe/(Mo+S) atomic ratios.

Next, several control experiments were performed, including: (i)

bubbling Ar gas for 2 h applying a potential of  $-0.2$  V vs. RHE using the MoS<sub>2</sub>-Fe-1 catalyst as the working electrode; (ii) N<sub>2</sub> gas was bubbled into the cell in an open circuit (OCP) for 2 h; (iii) the GDL electrode without the MoS<sub>2</sub>-Fe-1 catalyst, (iv) only 0.1 M Na<sub>2</sub>SO<sub>4</sub> electrolyte without Ar/N<sub>2</sub> gas or applied voltage and (v) N<sub>2</sub> steam treated with oxidizing trapper (alkaline KMnO<sub>4</sub>) and acid trapper (1 mM H<sub>2</sub>SO<sub>4</sub>).

As can be seen in Fig. 4f, when either Ar gas was used instead of N<sub>2</sub> gas or the catalyst-free GDL electrode was used, a negligible amount of NH<sub>3</sub> was detected. Insignificant amounts of NH<sub>3</sub> were detected at the OCP and in the 0.1 M Na<sub>2</sub>SO<sub>4</sub> electrolyte. Similarly, there is no significant difference in the absorbance values of the electrolyte purged with N<sub>2</sub> with and without treatment (Fig. S11), indicating low contamination of the supplied gas. This is corroborated by the spectra for NO<sub>x</sub> determination in N<sub>2</sub>-saturated 0.1 M Na<sub>2</sub>SO<sub>4</sub> (Figs. S12 and S13). These results suggest that NH<sub>3</sub> was produced by N<sub>2</sub> reduction in the presence of the GDL/MoS<sub>2</sub>-Fe catalysts rather than the sources of contamination.



**Fig. 6.** (a) time-dependent current density curve at  $-0.2$  V for GDL/MoS<sub>2</sub>-Fe-1 in different cycles of NRR. (b) NH<sub>3</sub> yields and FEs for GDL/MoS<sub>2</sub>-Fe-1 with recycling test at  $-0.2$  V vs. RHE. SEM images before (c) and after (d) the cycling stability test. (e) X-ray diffraction patterns for GDL/MoS<sub>2</sub>-Fe-1 catalyst before and after cycling stability test.

The influence of N<sub>2</sub> flow rate on electrocatalytic NRR was also investigated. Figure S14 shows that FE and NH<sub>3</sub> yield rates are unaffected when the N<sub>2</sub> flow rate increases from 20 to 60 mL min<sup>-1</sup>. This result suggests that the rate reduction is impartial to the gas-solid interface. Moreover, since the speed of the electrocatalytic reaction is independent of N<sub>2</sub> concentration, the diffusion of N<sub>2</sub> is not the decisive step of the reaction.

*In situ* electrochemical FTIR experiments are also conducted to elucidate the reaction mechanism of the NRR over the GDL/MoS<sub>2</sub>-Fe-1 at  $-0.2$  V vs RHE in 0.1 M Na<sub>2</sub>SO<sub>4</sub> solution (Fig. 5).

Different from the spectra in Ar (Fig. 5a), the spectra in N<sub>2</sub> for GDL/MoS<sub>2</sub> (Fig. 5b) have three extra negative-going peaks located at 1311, 1455 and 1560 cm<sup>-1</sup>, which are assigned to H-N-H wagging, -NH<sub>2</sub>

wagging and H-N-H bending, respectively, with the peak intensity increasing with increasing reaction time [48–50]. This result suggests the N≡N triple bond is cleaved into a single bond within the catalyst/electrolyte interface with the formation of -NH<sub>x</sub> intermediate on the surface of GDL/MoS<sub>2</sub>-Fe during the NRR.

Thus, based on the FTIR data and supported by several DFT studies [12,21,47,51–53] a possible mechanism was proposed (Fig. 5c), suggesting that ammonia synthesis follows the associative mechanism. In depth, N<sub>2</sub> is firstly adsorbed on the surface of the catalysts (I), and then a proton is attached to N<sub>2</sub> to form a \*NNH bond (II), which initially activates cleavage of N≡N bond.

In the subsequent step, the further hydrogenation process can undergo the formation of \*NNH<sub>2</sub>, following a distal pathway or via an



alternative pathway with the formation of \*NHNH. However, Ma et al. [21] founded that the  $\Delta G$  values on  $\text{Fe}_2\text{O}_3/\text{MoS}_2$  for the formation of \*NNH<sub>2</sub> species are lower than \*NHNH, indicating that associative distal mechanism is the favorable pathway for (III). In addition, no absorption of  $\text{N}_2\text{H}_4$ , an intermediate in the alternating route of NRR has been detected in the UV/Vis spectra of the catalysts (Fig. S9), suggesting the NRR reaction also occurred in our GDL/ $\text{MoS}_2\text{-Fe}_x\text{O}_y$  catalyst by the distal route mechanism [53].

After the first  $\text{NH}_3$  desorption, the remaining nitrogen atom is negatively charged, as is beneficial for the approaching of the next H atom and further nitrogen reduction (IV). Finally, the continuous electron transfer and hydrogenation (V-VII), the formation and desorption of ammonia occur on the surface of the GDL/ $\text{MoS}_2\text{-Fe-1}$  catalyst (VI).

Finally, the produced  $\text{NH}_3$  can be easily dissolved in water, which is helpful for the release of  $\text{NH}_3$  from the catalyst's surface, and the recovered active site can catalyze the next reaction cycle [52]. Therefore, the addition of  $\text{Fe}_x\text{O}_y$  to  $\text{MoS}_2$  is an efficient strategy for enhancing NRR activity.

Table 1 summarizes the results from this study with previous data on  $\text{NH}_3$  production and FE from the literature focused on  $\text{MoS}_2$  electrocatalysts. Direct comparison of the results from different research groups is avoided because of the difference in experimental conditions and the absence of a self-consistent set of metrics for the  $\text{NH}_3$  yield rates.

Nevertheless, the  $\text{NH}_3$  yields and FE in the present study are positive, indicating that the amorphous nature of  $\text{MoS}_2$  with a higher number of defects inducing more active site for  $\text{N}_2$  fixation [54] combined with  $\text{Fe}_x\text{O}_y$  acting as an  $\text{H}^+$  channel as a promising catalyst for  $\text{NH}_3$  production.

Stability is another key criterion for evaluating catalyst performance. To prove the stability of the catalyst, GDL/ $\text{MoS}_2\text{-Fe-1}$  was submitted to consecutive recycling electrolysis at  $-0.2$  V vs. RHE (Fig. 6). Fig. 6a shows the time-dependent current density curves for GDL/ $\text{MoS}_2\text{-Fe-1}$  in 6 cycles of NRR. As observed, the current density is not significantly reduced. The corresponding  $\text{NH}_3$  yield rates and FE (Fig. 6b) retain almost 93 % of their original values, suggesting that the GDL/ $\text{MoS}_2\text{-Fe-1}$  catalyst exhibits high stability and repeatable NRR performance during the recycling test.

After the recycling test, the SEM images (Fig. 6c, 6d) show that the structure and surface morphology of GDL/ $\text{MoS}_2\text{-Fe-1}$  hardly changed after recycling testing, and XRD analysis (Fig. 6e) confirms that GDL/ $\text{MoS}_2\text{-Fe-1}$  retains its amorphous structure. The EDX mapping (Fig. S15a–S15c) suggests that the  $\text{Fe}/\text{Fe}_x\text{O}_y$  species are uniformly dispersed on  $\text{MoS}_2$ . Also, the atomic ratio of S/Mo and  $\text{Fe}/(\text{Mo}+\text{S})$  is calculated to be 1.92 and 0.43 (Fig. S15d), respectively, demonstrating no dissolution of Fe or  $\text{MoS}_2$  species in the electrolysis process.

#### 4. Conclusions

In summary, amorphous  $\text{MoS}_2\text{-Fe}_x\text{O}_y$  catalysts supported by GDL substrate were successfully synthesized via a simple and low-cost electrodeposition method and tested for electrochemical  $\text{N}_2$  reduction under ambient conditions.

Physical characterization revealed the amorphous nature of the catalysts. Besides, their chemical state indicated the stoichiometric  $\text{MoS}_2$  and oxidized Fe species. Different compositions of GDL/ $\text{MoS}_2\text{-Fe}$  were tested. However, the GDL/ $\text{MoS}_2\text{-Fe-1}$ , with the lowest Fe content, was the more active catalyst for  $\text{NH}_3$  production, attaining  $7.38 \mu\text{mol h}^{-1} \text{cm}^{-2}$  and a corresponding Faradaic efficiency of 54.9 % at  $-0.2$  V vs. RHE in  $0.1 \text{ M Na}_2\text{SO}_4$ , values almost 2 times higher than GDL/ $\text{MoS}_2$  catalyst. The amorphous structure of  $\text{MoS}_2$  can provide a higher number of active sites, while  $\text{Fe}_x\text{O}_y$  can affect the electronic structure of  $\text{MoS}_2$ , facilitating  $\text{N}_2$  adsorption and acting as an  $\text{H}^+$  channel to promote NRR. In addition, the catalyst displayed high stability and durability, retaining almost 93 % of its original values after recycling tests.

This study not only provides an exciting earth-abundant catalyst for  $\text{NH}_3$  production at mild conditions but also opens up a promising

opportunity to synthesize amorphous materials for  $\text{N}_2$  fixation.

#### CRedit authorship contribution statement

**Caio V.S. Almeida:** Conceptualization, Investigation, Methodology, Formal analysis, Data curation, Funding acquisition, Writing – original draft. **Lucia H. Mascaro:** Supervision, Conceptualization, Funding acquisition, Writing – review & editing.

#### Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

#### Data availability

Data will be made available on request.

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#### Supplementary materials

Supplementary material associated with this article can be found, in the online version, at doi:10.1016/j.electacta.2023.143680.

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